

VISUALMESA™

ENERGY PERFORMANCE REAL-TIME OPTIMIZATION



Energy intensive manufacturers around the world are highly interested in, and have a strong need for, energy management systems (EMS) that will help them consume less energy and reduce their operational costs. Additionally, there is an increasing trend to optimize the mix of conventional and alternative energy sources used by facilities, which can help to protect the environment by reducing the emissions of gases such as CO₂ and NO_x.

Tradeoffs between the electrical, steam, and chilled water systems are determined by complex relationships that present an overwhelming 24/7/365 challenge to operators in their effort to provide stable and reliable service while at the same time trying to minimize cost and greenhouse gas emissions.

VisualMesa™ Energy Performance Real-Time Optimization (EP-RTO), using best in class technology, determines how to manage your steam, chilled water, electrical and fuel efficiently and reliably, and provides significant cost savings through the economic optimization.

EP-RTO is an online and real-time implementation with an engineering model, which considers plant control strategies and system reaction to changes in the utilities. EP-RTO gives operators actionable advice on how best to operate complex, interactive utility systems to minimize utility cost. For example, operators receive directives on how to set cogeneration and boiler steam production, swapping steam/electric drives, chilled water supply, the export of steam, and how to manage real-time power purchase and sale.

Benefits

Reducing Energy Cost against Greenhouse Gas Emissions to help meet Environmental Sustainability Goals

Managing Facility* Steam, Chilled Water, Electricity & Fuel

Optimizing Energy Cost within Emissions† Constraints

Actionable Advice that Reduces Energy Spend

Facility planning through “What-If” case study capability

Attractive ROI (typical payback less than 1 year)

Reducing Carbon Tax and Improve Cap & Trade (local laws)

Technology Advantages

Online Engineering Model and Real-Time Optimization

Rigorous Combustion and Emissions Model

Mixed Integer, Non-linear Optimizer

Robust Integration with Utility Systems & Facility IT Systems

Easy to Use, Export to Excel

Familiar Microsoft Visio Based User Interface

Representative Reduction in Energy Spend and Greenhouse Gas Emissions

3% to 6% Energy Savings in Open-loop Optimization Advisory Mode

5% to 12% Energy Savings in Closed-loop Optimization

1% to 3% Energy Savings from KPIs

Typical Savings in 100,000 bbl/d US Refinery

\$1MM to \$2MM/Year Steam Imbalance resolution

Greater than \$2MM/Year of integrated Steam/Power/Fuels/Hydrogen systems management

\$2MM to \$5MM/Year Carbon Tax or Trading (jurisdiction dependent; i.e., California's Cap-and-Trade Program)

Reduced CAPEX through accurate and efficient case study analysis



Operational Excellence & Collaboration

Empowering Stakeholder Collaboration

Visibility into Steam, Electric, Chilled Water & Fuel Systems

Recommendations for Minimum Cost Utility Supply Operation

“What If” Studies: Predict the Impact of Proposed Changes

Auditing, Accounting & Data Validation

Industry Experience

Refining & Petrochemicals

Campus & District Energy

Sugar & Ethanol

Pulp & Paper

Representative Case Histories

ExxonMobil

Phillips 66

Chevron

Usacucar

Repsol

KNPC

Total

Thermal Energy Storage

DOW (Rohm & Hass)

Cepsa Quimica

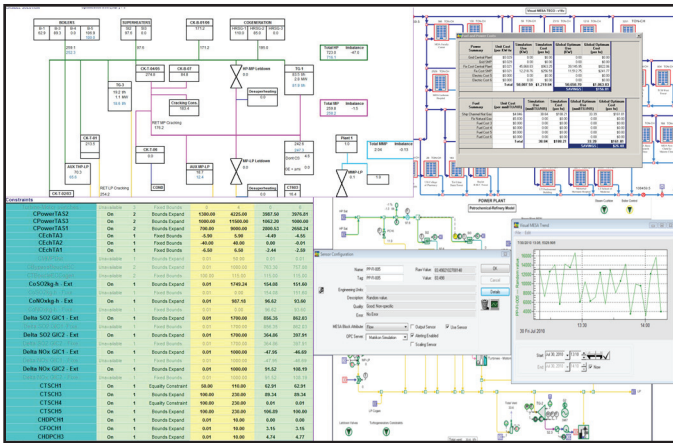
Air Liquide

LOTOS

INEOS

YPF

Detailed Report of Recommended Operational Changes



EP-RTO also determines where to make incremental steam and electricity as well as identifying which turbines or valves will most efficiently let down the steam between process levels.

VisualMesa™ The Plant Refinery Energy Performance Real-Time Optimization

Regeneration Power Plant Cracking Plants 1-7 Tanks Refinery

Unit Cost (\$/hr) Fuel Use (ton/hr) Power Use (MW)

Economic Summary

	Simulation (per hr)	Global Optimum (per hr)	Savings (per hr)
Fuel Summary			
FO high naph	\$27,874	\$0.00	\$0.00
FO low naph	\$28,112	\$6.63	\$2,772.89
NS Cost 1	\$38,000	\$0.00	\$2,862.21
NS Cost 2	\$36,000	\$0.00	\$0.00
NS Cost 3	\$38,000	\$19.49	\$3,660.76
CA	\$11,364	6.38	\$71.18
Total	335.25	\$3,956.93	\$17,735.18
Power Summary			
Grid	\$0.00	\$0.00	\$0.00
Penalty for not in contact (E)	\$0.013	\$0.00	\$0.00
Penalty for not in contact (E) range	\$0.00	\$0.00	\$0.00
Electric Cost 4	\$0.00	\$0.00	\$0.00
Electric Cost 5	\$0.00	\$0.00	\$0.00
Electric Cost 6	\$0.00	\$0.00	\$0.00
Total	\$5,260.00	\$2,715.00	\$2,545.00
Other Cost			
Denaturalized water	\$17,400	\$740.01	\$7,237.27
CPCO-Ranger1	\$0.00	\$8.13	\$0.00
CPCO-Ranger2	\$30,000	\$0.00	\$0.00
CPCO-Ranger3	\$15,000	\$0.00	\$0.00
Emissions cost	\$45,000	\$6.94	\$6.82
Dummy Fuel Cost	\$0.00	\$0.00	\$0.00
Total	\$747.07	\$740.23	\$6.84
Global Optimum			
Simulation	\$12,819.61	\$12,688.72	\$150.08

Constraints such as: Total Energy Required & Emissions

FULL SYSTEM
Visual MESA Demo Model

SOLIDS
Visual MESA Demo Model

Solids Stack
Visual MESA Demo Model

Emissions Results Table:

Inputs	Flue Gas Properties	Emissions Components	Description
Simulation Output			
	Mass (Lb/Hr)	Mass/Duty (Lb/MMBTU)	Mass/Volume (Lb/MMSCF)
	Concentration (mass %)	Concentration (mass %)	Concentration (vol %)
Carbon Dioxide	7.7237	0.1316	0.0317
Sulfur Dioxide	0.1054	0.0019	1.800E-4
Nitrogen Oxide	1.5210E-6	2.2900E-9	2.6600E-9
			2.8476E-6

Optimization Output

Local

	Mass (Lb/Hr)	Mass/Duty (Lb/MMBTU)	Mass/Volume (Lb/MMSCF)	Concentration (mass %)	Concentration (vol %)
Carbon Dioxide	5.9718	0.1316	0.0317	15.4794	1
Sulfur Dioxide	0.0809	0.0019	1.8000E-4	0.2112	1
Nitrogen Oxide	1.0120E-6	2.2900E-9	2.0860E-9	2.6476E-6	1.66

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